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EP 0 153 176 B1

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## Description

Mineral oils containing paraffin wax have the characteristic of becoming less fluid as the temperature of the oil decreases. This loss of fluidity is due to the crystallization of the wax into plate-like crystals which eventually form a spongy mass entrapping the oil therein.

It has long been known that various additives act as wax crystal modifiers when blended with waxy mineral oils. These compositions modify the size and shape of wax crystals and reduce the adhesive forces between the crystals and between the wax and the oil in such a manner as to permit the oil to remain fluid at a lower temperature.

Various pour point depressants have been described in the literature and several of these are in commercial use. For example, U.S. Pat. No. 3,048,479 teaches the use of copolymers of ethylene and C<sub>3</sub>-C<sub>5</sub> vinyl esters, e.g. vinyl acetate, as pour depressants for fuels, specifically heating oils, diesel and jet fuels. Hydrocarbon polymeric pour depressants based on ethylene and higher alpha-olefins, e.g. propylene, are also known. U.S. Patent 3,961,916 teaches the use of a mixture of copolymers, one of which is a wax crystal nucleator and the other a growth arrestor to control the size of the wax crystals.

United Kingdom Patent 1263152 suggests that the size of the wax crystals may be controlled by using a copolymer having a lower degree of side chain branching.

It has also been proposed in for example United Kingdom Patent 1469016 that the copolymers of di-n-alkyl fumarates and vinyl acetate which have previously been used as pour depressants for lubricating oils may be used as co-additives with ethylene/vinyl acetate copolymers in the treatment of distillate fuels with high final boiling points to improve their low temperature flow properties. According to United Kingdom Patent 1469016 these polymers may be C<sub>6</sub> to C<sub>18</sub> alkyl esters of unsaturated C<sub>4</sub> to C<sub>8</sub> dicarboxylic acids particularly lauryl fumarate and lauryl-hexadecyl fumarate. Typically the materials used are mixed esters with an average of about 12 carbon atoms (Polymer A). It is notable that the additives are shown not to be effective in the "conventional" fuels of lower Final Boiling Point (Fuels III and IV).

United States Patent 3252771 relates to the use of polymers of C<sub>16</sub> to C<sub>18</sub> alpha-olefines obtained by polymerising olefin mixtures that predominate in normal C<sub>16</sub> to C<sub>18</sub> alpha-olefines with aluminium trichloride/alkyl halide catalysts as pour point and cloud point depressants in distillate fuels of the broad boiling, easy to treat types available in the United States in the early 1960's.

With the increasing diversity in distillate fuels, types of fuel have emerged which cannot be treated by the existing additives or which require an uneconomically high level of additive to achieve the necessary reduction in their pour point and control of wax crystal size for low temperature filterability to allow them to be used commercially. One particular group of fuels that present such problems are those which have a relatively narrow, and/or low boiling range. Fuels are frequently characterised by their Initial Boiling Point, Final Boiling Point and the interim temperatures at which certain volume percentages of the initial fuel have been distilled. Fuels whose 20% to 90% distillation point differ within the range of from 70 to 100°C and/or whose 90% boiling temperature is from 10 to 25°C of the final boiling point and/or whose final boiling points are between 340 and 370°C have been found particularly difficult to treat sometimes being virtually unaffected by additives or otherwise requiring very high levels of additive. All distillations referred to herein are according to ASTM D86.

With the increase in the cost of crude oil, it has also become important for a refiner to increase his production of distillate fuels and to optimise his operations using what is known as sharp fractionation again resulting in distillate fuels that are difficult to treat with conventional additives or that require a treat level that is unacceptably high from the economic standpoint. Typical sharply fractionated fuels have a 90% to final boiling point range of 10 to 25°C usually with a 20 to 90% boiling range of less than 100°C, generally 50 to 100°C. Both types of fuel have final boiling points above 340°C generally a final boiling point in the range 340°C to 370°C especially 340°C to 365°C.

The copolymers of ethylene and vinyl acetate which have found widespread use for improving the flow of the previously widely available distillate fuels have not been found to be effective in the treatment of the narrow boiling and/or sharply fractionated fuels described above. Furthermore use of mixtures as illustrated in United Kingdom Patent 1469016 have not been found effective.

We have found however that polymers and copolymers containing very specific alkyl groups, such as specific di-n-alkyl fumarate/vinyl acetate copolymers, are effective in both lowering the pour point of the difficult to treat fuels described above and controlling the size of the wax crystals to allow filterability including those fuels of the lower final boiling point in which the additives of United Kingdom Patent 1469016 were ineffective.

Specifically we have found that the average number of carbon atoms in the alkyl groups in the polymer or copolymer must be from 12 to 14 and that no more than 10 wt% of the alkyl groups should contain more

than 14 carbon atoms and preferably no more than 20 wt% of the alkyl groups contain fewer than 12 carbon atoms. These polymers are particularly effective when used in combination with other low temperature flow improvers which on their own are ineffective in these types of fuels. Our parallel European Patent Application 85301048.6 Publication Number 0153177 relates to the use of this type of copolymer in combination with other flow improving compounds.

The present invention therefore provides the use for improving the flow properties of a distillate petroleum fuel oil boiling in the range 120°C to 500°C whose 90% to final boiling point range is 10 to 25°C and preferably, whose 20% and 90% distillation points differ by less than 100°C or preferably whose final boiling point is in the range 340°C to 370°C of an additive comprising a polymer containing at least 25 wt% of n-alkyl groups, the average number of carbon atoms in the n-alkyl groups is from 12 to 14 and no more than 10 wt% of the alkyl groups contain more than 14 carbon atoms and preferably no more than 20 wt% of the alkyl groups contain fewer than 12 carbon atoms.

The additives are preferably used in an amount from 0.0001 to 0.5 wt%, preferably 0.001 and 0.2 wt% based on the weight of the distillation petroleum fuel oil, and the present invention also includes such treated distillate fuel.

The preferred polymer is a copolymer containing at least 25 preferably at least 50 wt.% more preferably from 75 to 90 wt.% of a di-n alkyl ester of a dicarboxylic acid containing alkyl groups containing an average of 12 to 14 carbon atoms and 10 to 50 wt.% of another unsaturated ester such as a vinyl ester and/or an alkyl acrylate, methacrylate or alpha olefine. Equimolar copolymers of a di-n-alkyl fumarate and vinyl acetate are particularly preferred.

The polymers or copolymers used in the present invention preferably have a number average molecular weight in the range of 1000 to 100,000, preferably 1,000 to 30,000 as measured, for example, by Vapor Pressure Osmometry.

The carboxylic acid esters useful for preparing the preferred polymer can be represented by the general formula:



where in  $R_1$  and  $R_2$  are hydrogen or a  $C_1$  to  $C_4$  alkyl group, e.g., methyl,  $R_3$  is the  $C_{12}$  to  $C_{14}$  average, straight chain alkyl group, and  $R_4$  is  $COOR_3$ . These may be prepared by esterifying the particular dicarboxylic acid with the appropriate alcohol or mixture of alcohols.

Other unsaturated esters, which can be copolymerized are the  $C_{12}$ - $C_{14}$  alkyl acrylates and methacrylates.

The dicarboxylic acid di- ester monomers may be copolymerized with various amounts, e.g., 5 to 70 mole %, of other unsaturated esters or olefins. Such other esters include short chain alkyl esters having the formula:



where  $R'$  is hydrogen or a  $C_1$  to  $C_4$  alkyl group,  $R''$  is  $-COOR''''$  or  $-OOCR''''$  where  $R''''$  is a  $C_1$  to  $C_5$  alkyl group branched or unbranched, and  $R'''$  is  $R''$  or hydrogen. Examples of these short chain esters are

methacrylates, acrylates, the vinyl esters such as vinyl acetate and vinyl propionate being preferred. More specific examples include methyl methacrylate, isopropenyl acetate and butyl and isobutyl acrylate.

Our preferred copolymers contain from 40 to 60 mol % of a C<sub>12</sub>-C<sub>14</sub> average dialkyl fumarate and 60 to 40 mole % of vinyl acetate.

Where ester polymers or copolymers are used they may conveniently be prepared by polymerising the ester monomers in a solution of a hydrocarbon solvent such as heptane, benzene, cyclohexane, or white oil, at a temperature generally in the range of from 20°C to 150°C and usually promoted with a peroxide or azo type catalyst, such as benzoyl peroxide or azodi-isobutyronitrile, under a blanket of an inert gas such as nitrogen or carbon dioxide, in order to exclude oxygen.

The additives of the present invention are particularly effective when used in combination with other additives known for improving the cold flow properties of distillate fuels generally, although they may be used on their own to impart a combination of improvements to the cold flow behaviour of the fuel.

The additives of the present invention are particularly effective when used with the polyoxyalkylene esters, ethers, ester/ethers and mixtures thereof, particularly those containing at least one, preferably at least two C<sub>10</sub> to C<sub>30</sub> linear saturated alkyl groups and a polyoxyalkylene glycol group of molecular weight 100 to 5,000 preferably 200 to 5,000, the alkyl group in said polyoxyalkylene glycol containing from 1 to 4 carbon atoms. These materials form the subject of European Patent Publication 0061895 A2.

The preferred esters, ethers or ester/ethers useful in the present invention may be structurally depicted by the formula:



where R and R<sup>1</sup> are the same or different and may be

(i) n-Alkyl

O

"

(ii) n-Alkyl - C

O

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(iii) n-Alkyl -O-C-(CH<sub>2</sub>)<sub>n</sub>-

O

O

"

"

(iv) n-Alkyl -O-C-(CH<sub>2</sub>)<sub>n</sub>-C-

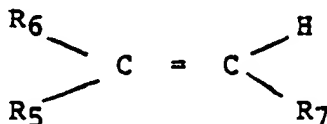
the alkyl group being linear and saturated and containing 10 to 30 carbon atoms, and A represents the polyoxyalkylene segment of the glycol in which the alkylene group has 1 to 4 carbon atoms, such as a polyoxymethylene, polyoxyethylene or polyoxytrimethylene moiety which is substantially linear; some degree of branching with lower alkyl side chains (such as in polyoxypropylene glycol) may be tolerated but it is preferred the glycol should be substantially linear.

Suitable glycols generally are the substantially linear polyethylene glycols (PEG) and polypropylene glycols (PPG) having a molecular weight of about 100 to 5,000 preferably about 200 to 2,000. Esters are preferred and fatty acids containing from 10-30 carbon atoms are useful for reacting with the glycols to form the ester additives and it is preferred to use a C<sub>18</sub>-C<sub>24</sub> fatty acid, especially behenic acids, the esters may also be prepared by esterifying polyethoxylated fatty acids or polyethoxylated alcohols.

Polyoxyalkylene diesters, diethers, ether/esters and mixtures thereof are suitable as additives with diesters preferred for use in narrow boiling distillates whilst minor amounts of monoethers and monoesters may also be present and are often formed in the manufacturing process. It is important for additive performance that a major amount of the dialkyl compound is present. In particular stearic or behenic diesters of polyethylene glycol, polypropylene glycol or polyethylene/polypropylene glycol mixtures are

preferred.

The additives of this invention may also be used with the ethylene unsaturated ester copolymer flow improvers. The unsaturated monomers which may be copolymerized with ethylene, include unsaturated mono and diesters of the general formula:



wherein  $\text{R}_6$  is hydrogen or methyl;  $\text{R}_5$  is a  $-\text{OOCR}_8$  group wherein  $\text{R}_8$  is hydrogen or a  $\text{C}_1$  to  $\text{C}_{28}$ , more usually  $\text{C}_1$  to  $\text{C}_{17}$ , and preferably a  $\text{C}_1$  to  $\text{C}_8$ , straight or branched chain alkyl group; or  $\text{R}_5$  is a  $-\text{COOR}_8$  group wherein  $\text{R}_8$  is as previously described but is not hydrogen and  $\text{R}_7$  is hydrogen or  $-\text{COOR}_8$  as previously defined. The monomer, when  $\text{R}_5$  and  $\text{R}_7$  are hydrogen and  $\text{R}_6$  is  $-\text{OOCR}_8$ , includes vinyl alcohol esters of  $\text{C}_1$  to  $\text{C}_{29}$ , more usually  $\text{C}_1$  to  $\text{C}_{18}$ , monocarboxylic acid, and preferably  $\text{C}_2$  to  $\text{C}_5$  monocarboxylic acid. Examples of vinyl esters which may be copolymerised with ethylene include vinyl acetate, vinyl propionate and vinyl butyrate or isobutyrate, vinyl acetate being preferred. We prefer that the copolymers contain from 20 to 40 wt.% of the vinyl ester more preferably from 25 to 35 wt.% vinyl ester. They may also be mixtures of two copolymers such as those described in United States Patent 3961916.

It is preferred that these copolymers have a number average molecular weight as measured by vapor phase osmometry of 1000 to 6000, preferably 1000 to 3000.

The additives of the present invention may also be used in distillate fuels in combination with polar compounds, either ionic or nonionic, which have the capability in fuels of acting as wax crystal growth inhibitors. Polar nitrogen containing compounds have been found to be especially effective when used in combination with the glycol esters, ethers or ester/ethers and such three component mixtures are within the scope of the present invention. These polar compounds are generally amine salts and/or amides formed by reaction of at least one molar proportion of hydrocarbyl substituted amines with a molar proportion of hydrocarbyl acid having 1 to 4 carboxylic acid groups or their anhydrides; ester/amides may also be used contain 30 to 300 preferably 50 to 150 total carbon atoms. These nitrogen compounds are described in U.S. Patent 4,211,534. Suitable amines are usually long chain  $\text{C}_{12}$ - $\text{C}_{40}$  primary, secondary, tertiary or quaternary amines or mixtures thereof but shorter chain amines may be used provided the resulting nitrogen compound is oil soluble and therefore normally containing about 30 to 300 total carbon atoms. The nitrogen compound preferably contains at least one straight chain  $\text{C}_8$ - $\text{C}_{40}$  preferably  $\text{C}_{14}$  to  $\text{C}_{24}$  alkyl segment.

Suitable amines include primary, secondary, tertiary or quaternary, but preferably are secondary. Tertiary and quaternary amines can only form amine salts. Examples of amines include tetradecyl amine, cocoamine, hydrogenated tallow amine and the like. Examples of secondary amines include dioctadecyl amine, methyl-behenyl amine and the like. Amine mixtures are also suitable and many amines derived from natural materials are mixtures. The preferred amine is a secondary hydrogenated tallow amine of the formula  $\text{HNR}_1\text{R}_2$  wherein  $\text{R}_1$  and  $\text{R}_2$  are alkyl groups derived from hydrogenated tallow fat composed of approximately 4%  $\text{C}_{14}$ , 31%  $\text{C}_{16}$ , 59%  $\text{C}_{18}$ .

Examples of suitable carboxylic acids for preparing these nitrogen compounds (and their anhydrides) include cyclo-hexane 1,2 dicarboxylic acid, cyclohexene dicarboxylic acid, cyclopentane 1,2 dicarboxylic acid, naphthalene dicarboxylic acid and the like. Generally these acids will have about 5-13 carbon atoms in the cyclic moiety. Preferred acids useful in the present invention are benzene dicarboxylic acids such as ortho-phthalic acid, para-phthalic acid, and meta-phthalic acid. Ortho-phthalic acid or its anhydride is particularly preferred. The particularly preferred compound is the amide-amine salt formed by reacting 1 molar portion of phthalic anhydride with 2 molar portions of di-hydrogenated tallow amine. Another preferred compound is the diamide formed by dehydrating this amide-amine salt.

The relative proportions of additives used in the mixtures are from 0.5 to 20 parts by weight of the polymer of the invention containing the n-alkyl groups containing an average of 12 to 14 carbon atoms to 1 part of the other additives such as the polyoxyalkylene esters, ether or ester/ether, more preferably from 1.5 to 9 parts by weight of the polymer of the invention.

The additive systems of the present invention may conveniently be supplied as concentrates for incorporation into the bulk distillate fuel. These concentrates may also contain other additives as required. These concentrates preferably contain from 3 to 75 wt.%, more preferably 3 to 60 wt.%, most preferably 10 to 50 wt.% of the additives preferably in solution in oil. Such concentrates are also within the scope of the

present invention.

The present invention is illustrated by the following Examples in which the effectiveness of the additives of the present invention as pour point depressants and filterability improvers were compared with other similar additives in the following tests.

5 By one method, the response of the oil to the additives was measured by the Cold Filter Plugging Point Test (CFPP) which is carried out by the procedure described in detail in "Journal of the Institute of Petroleum", Volume 52, Number 510, June 1966, pp. 173-185. This test is designed to correlate with the cold flow of a middle distillate in automotive diesels.

10 In brief, a 40 ml sample of the oil to be tested is cooled in a bath which is maintained at about  $-34^{\circ}\text{C}$  to give non-linear cooling at about  $1^{\circ}\text{C}/\text{min}$ . Periodically (at each one degree Centigrade drop in temperature starting from at least  $2^{\circ}\text{C}$  above the cloud point) the cooled oil is tested for its ability to flow through a fine screen in a prescribed time period using a test device which is a pipette to whose lower end is attached an inverted funnel which is positioned below the surface of the oil to be tested. Stretched across the mouth of the funnel is a 350 mesh screen having an area defined by a 12 millimetre diameter. The periodic tests are  
15 each initiated by applying a vacuum to the upper end of the pipette whereby oil is drawn through the screen up into the pipette to a mark indicating 20 ml of oil. After each successful passage the oil is returned immediately to the CFPP tube. The test is repeated with each one degree drop in temperature until the oil fails to fill the pipette within 60 seconds. This temperature is reported as the CFPP temperature. The difference between the CFPP of an additive free fuel and of the same fuel containing additive is reported as  
20 the CFPP depression by the additive. A more effective flow improver gives a greater CFPP depression at the same concentration of additive.

Another determination of flow improver effectiveness is made under conditions of the flow improver distillate operability test (DOT test) which is a slow cooling test designed to correlate with the pumping of a stored heating oil. In this test the cold flow properties of the described fuels containing the additives were  
25 determined by the DOT test as follows. 300 ml of fuel are cooled linearly at  $1^{\circ}\text{C}/\text{hour}$  to the test temperature and the temperature then held constant. After 2 hours at the test temperature, approximately 20 ml of the surface layer is removed as the abnormally large wax crystals which tend to form on the oil/air interface during cooling. Wax which has settled in the bottle is dispersed by gentle stirring, then a CFPP filter assembly is inserted. The tap is opened to apply a vacuum of 500 mm of mercury, and closed when  
30 200 ml of fuel have passed through 1 the filter into the graduated receiver. A PASS is recorded if the 200 ml are collected within ten seconds through a given mesh size or a FAIL if the flow rate is too slow indicating that the filter has become blocked.

CFPP filter assemblies with filter screens of 20, 30, 40, 60, 80, 100, 120, 150, 200, 250 and 350 mesh number are used to determine the finest mesh (largest mesh number) the fuel will pass. The larger the  
35 mesh number that a wax containing fuel will pass, the smaller are the wax crystals and the greater the effectiveness of the additive flow improver. It should be noted that no two fuels will give exactly the same test results at the same treatment level for the same flow improver additive.

The Pour Point was determined by two methods, either the ASTM D 97 or a visual method in which 100 ml samples of fuel in a 150 ml narrow necked bottle containing the additive under test, are cooled at  
40  $1^{\circ}\text{C}/\text{hour}$  from  $5^{\circ}\text{C}$  above the wax appearance temperature. The fuel samples were examined at  $3^{\circ}\text{C}$  intervals for their ability to pour when tilted or inverted. A fluid sample (designated F) would move readily on tilting, a semi-fluid (designated semi-F) sample may need to be almost inverted, while a solid sample (designated S) can be inverted with no movement of the sample.

The fuels used in these Examples were:

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	Fuel	ASTM-D-86 Distillation, °C			
		Wax Appearance Point	Initial Boiling Point	20% 90%	Final Boiling Point
5					
	A	-5	202	270	328
10	B	-2	202	254	340
	C	-2.5	274	286	330
	D	-4	155	215	335
15	E	-1.5	196	236	344

The Additives used were as follows:

Additive 1: A polyethylene glycol of 400 average molecular weight esterified with 2 moles of behenic acid.

20 Additive 2: A copolymer of a mixed C<sub>12</sub>/C<sub>14</sub> alkyl fumarate obtained by reaction of 50:50 weight mixture of normal C<sub>12</sub> and C<sub>14</sub> alcohols with fumaric acid and vinyl acetate prepared by solution copolymerisation of a 1 to 1 mole ratio mixture at 60 °C using azo diisobutyronitrile as catalyst.

The results in the CFPP and Pour Point tests were as follows:

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	Fuel	Additiv	Amount ppm	ASTM D 97	
				CFPP Depression	Pour Point
5					
	A	None		-5°C	-9°C
		1	500	-8°C	-6°C
10		2	500	-3°C	-15°C
		2:1	300:200	-9°C	-18°C
		2:1	600:400	-11°C	-18°C
15					
	B	None		-4°C	-6°C
		1	120		-6°C
20		1	300	-8°C	4°C
		2	180		-15°C
		2	300	-2°C	-2°C
25		2:1	180/120	-11°C	7
		2:1	300/200	-13°C	9
30	C	None		-4°C	-6°C
		1	500	-8°C	4
		1	1000	-7°C	3
		2	1000	-2°C	-2
35		2:1	300/200	-6°C	2
		2:1	600/400	-10°C	6
40					

The Use of Additive 1 as sole additive is not an Example of the invention.

45 The additives of the invention were compared in the DOT test with Additive 3 which was an oil solution containing 63 wt.% of a combination of polymers comprising 13 parts by weight of an ethylene/vinyl acetate copolymer of number average molecular weight 2500 and vinyl acetate content of 36 wt.% and 1 part by weight of a copolymer of ethylene and vinyl acetate of number average molecular weight 3500 and a vinyl acetate content of about 13 wt. %.

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DOT Testppm of additive to pass DOT (120 mesh) at -10°C

5	Fuel	Additive 3	Mixture of 3 Parts of 1 and 2 Parts of 2	
	A	>3,000	700	
10	B	800	250	
	C	1,500	700	
	D	1,250	500	
15	E	>1,500	300	

Various fumarate/vinyl acetate copolymers were tested in admixture (3 parts) with Additive 1 (2 parts) to determine the effect of the chain length in the fumarate with the following results.

20	Fuel	Alcohols used to make fumarate	Average C Number in fumarate	Pour Point Test Appearance at -10°C	CFPP Depression	
					500 ppm(ai)	1,000 ppm (ai)
	A	C-8	8	S	2	3
30		C-9	9	-	2	-
		C-10	10	S	3	3
		C-10/C-12	11	S	3	4
35		C-11	11	-	3	3
		C-12	12	S	3	4
		C-12/C-14	13	F	5	7
40		C-14	14	F	-2	-2

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	Fuel	Alcohols used to make fumarate	Average C Number in fumarate	Pour Point Test Appearance at -10°C	CFPP Depression 300 ppm
5	B	C-8	8	S	3
10		C-9	9	-	5
		C-10	10	S	4
		C-10/C-12	11	S	5
		C-11	11	-	5
15		C-12	12	S	3
		C-12/C-14	13	F	7
		C-14	14	F	0
20					
25					
					1,000 ppm
30	C	C-10	10		3
		C-10/C-12	11		3
		C-11	11		3
35		C-12	12		3
		C-12/C-14	13		6
		C-14	14		0
40		C-18	18		3

Various fumarate/vinyl acetate copolymers obtained from different alcohols but averaging 12 to 13.5 carbon atoms in the alkyl groups were tested in the same mixture as in the previous example in the CFPP and Visual pour point tests with the following results.

Fumarate Alcohols (All n-alcohols except oxo-C-13) ratio's by weight	Fuel A				Fuel B			Fuel C		
	Alcohol Average C-number	CFPP Depression		Pour Point Appearance at -10°C	CFPP Depression 300 ppm	500 ppm	Pour Point Appearance at -10°C	CFPP Depression 1000 ppm	Pour Point Appearance at -10°C	
		500 ppm	1000 ppm							
1. C-12/C-14 = 1/1	13.0	5	7	F	7	9	F	6	F	
2. C-12/C-14 = 3/1	12.5	2	4	Semi-F	6	6	Semi-F	3	-	
3. C-12/C-14 = 1/3	13.5	0	1	F	2	5	F	0	-	
4. C-10/C-16 = 1/1	13.0	-2	-1	F	2	1	F	1	-	
5. C-13 oxo (from tetrapropylene)	13.0	3	-	S	5	5	S	3	-	
6. C-12/C-14/C-16 = 2/1/1	13.5	1	-	-	1	-	-	0	-	
7. C-12/C-14/C-16 = 8/3/1	12.7	4	7	F	7	9	F	7	F	
8. C-8/C-10/C-12/C-14/C-16/C-18 = 9/11/36/30/10/4	12.2	4	6	F	4	7	F	2	F	
9. Ditto = 3/8/33/37/12/8	13.0	0	1	-	2	2	-	1	-	
10. C-12/C-14/C-16/C-18 = 45/38/12/5	13.4	0	0	-	2	2	-	1	-	
11. C-8 to C-18 = 13/10/41/15/9/13	12.5	2	3	-	4	6	-	1	-	

The fuels B and C were used in the following Examples together with

Fuel F	ASTM D-86 Distillation °C				
	IBP	20%	50%	90%	FBP
5	182	254	285	324	343

The results are CFPP and visual Pour Point results shown for various additives in the following table. Where the additive has no pour depressing effect the CFPP value is not measured because without pour depression the fuel cannot be used.

Fuel B			
CFPP Depression			
Additive	400 ppm	Fumarate vinyl acetate Additive 1	400 ppm fumarate/vinyl acetate Additive 1
Alcohol content of Fumarate	100 ppm		100 ppm Additive 3
C <sub>4</sub>			2
C <sub>6</sub>			2
C <sub>8</sub>			2
C <sub>9</sub>	No pour depression*		2
C <sub>10</sub>			2
C <sub>11</sub>			2
C <sub>12</sub>			2
C <sub>13</sub>	7°C		8
C <sub>14</sub>	0		2
C <sub>16</sub>	Raised by 2°C		Raised by 2°C
C <sub>18</sub>	No pour depression*		
C <sub>22</sub>			
Mixed C <sub>12</sub> /C <sub>14</sub>			
3:1	No effect		2
1:1	8°C		9
1:3	4°C		5
C <sub>18</sub> /C <sub>16</sub>	Raised by 1°C		Raised by 1°C
C <sub>10</sub> /C <sub>12</sub>	No effect		

\* No pour depression observed at -10°C after the 1°C/hour cool.

CFPP Depression

5	Additive	<u>Fuel C</u>	<u>Fuel F</u>	
		800 ppm F/VA 200 ppm Additive 1	800 ppm F/VA 200 ppm Additive 1	800 ppm F/VA 200 ppm 1 100 ppm 3
10	Alcohol content of Fumarate			
	C <sub>4</sub>			
	C <sub>6</sub>			
	C <sub>8</sub>			
	C <sub>9</sub>	No pour depression		
15	C <sub>10</sub>			
	C <sub>11</sub>			
	C <sub>12</sub>	3	9	4
	C <sub>13</sub>	0	1	1
	C <sub>14</sub>	0	2	
20	C <sub>16</sub>	No pour depression		
	C <sub>18</sub>			
	C <sub>22</sub>			
	Mixed C <sub>12</sub> /C <sub>14</sub>			
	3:1	No pour depression		1
25	1:1	4	10	8
	1:3	1	4	4
	C <sub>18</sub> /C <sub>16</sub>			
	1:1	0	0	1
30	C <sub>10</sub> /C <sub>12</sub>			
	1:1	No pour depression		

\* No pour depression observed at -10°C after the 1°C/hour cool.

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The Additives were also tested in combination with Additive 4 the half amide formed by reacting two moles of hydrogenated tallow amine with phthalic anhydride and the CFPP depressions in Fuel B were as follows

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45	Additive	CFPP Depressions
	Additive 4 (250 ppm)	6
	Additive 3 (100 ppm)	
	C <sub>12</sub> /C <sub>14</sub> F/VA (250 ppm)	
50	Additive 4 (300 ppm)	
	Additive 1 (100 ppm)	6
	C <sub>12</sub> /C <sub>14</sub> F/VA (100 ppm)	
55	Additive 4 (250 ppm)	0
	C <sub>12</sub> /C <sub>14</sub> F/VA (250 ppm)	

## Claims

Claims for the following Contracting States: BE CH DE FR GB IT LI NL SE

1. The use for improving the low temperature properties of a distillate petroleum fuel oil boiling in the range 120°C to 500°C, whose 90% to final boiling point range is 10 to 25°C of an additive comprising a polymer or copolymer of a di-n-alkyl ester of a mono-ethylenically unsaturated C<sub>4</sub> to C<sub>8</sub> dicarboxylic acid containing at least 25 wt.% of n-alkyl groups wherein the average number of carbon atoms in the n-alkyl groups is from above 12 to 14 and no more than 10 wt.% of alkyl groups in the copolymer containing more than 14 carbon atoms.
2. The use according to claim 1 in which the 20% to 90% distillation points differ by less than 100°C.
3. The use according to claim 1 or claim 2 in which the final boiling point is in the range 340°C to 370°C.
4. The use according to any of claims 1 to 3 in which no more than 20 wt.% of the alkyl group contains fewer than 12 carbon atoms.
5. The use according to any of claims 1 to 4 in which the copolymer is of a di-n-alkyl ester of dicarboxylic acid in which the alkyl groups containing an average of 12 to 14 carbon atoms and from 10 to 50 wt.% of a vinyl ester, an alkyl acrylate or methacrylate.
6. The use according to any of claims 1 to 4 in which there is also added a polyoxyalkylene ester, ether, ester/ether and mixtures thereof, containing at least two C<sub>10</sub> to C<sub>30</sub> linear saturated alkyl groups and a polyoxyalkylene glycol of molecular weight 100 to 5,000 preferably 200 to 5,000, the alkyl group in said polyoxyalkylene glycol containing from 1 to 4 carbon atoms.
7. The use according to any of claims 1 to 4 in which there is also added a polar compound, either ionic or nonionic, which has the capability in fuels of acting as wax crystal growth inhibitors.
8. The use according to claim 7 in which the polar compounds are the amine salts and/or amides formed by reaction of at least one molar proportion of hydrocarbyl-substituted amines with a molar proportion of hydrocarbyl acid having 1 to 4 carboxylic acid groups or their anhydrides containing a total of 30 to 300 carbon atoms.
9. The use according to any of claims 1 to 4 in which there is also added an ethylene/unsaturated ester copolymer.
10. A distillate petroleum fuel oil boiling in the range 120°C to 500°C whose 90% to final boiling point is 10 to 25°C containing from 0.001 to 0.5 wt.% of a polymer or copolymer of a di-n-alkyl ester of a mono-ethylenically unsaturated C<sub>4</sub> to C<sub>8</sub> dicarboxylic acid containing at least 25 wt.% of n-alkyl groups wherein the average number of carbon atoms in the n-alkyl groups is from above 12 to 14, there being present no more than 10 wt.% of alkyl groups containing more than 14 carbon atoms in the copolymer.
11. A distillate petroleum fuel oil according to claim 10 whose 20% and 90% distillation points differ by less than 100°C.
12. A distillate petroleum fuel oil according to claim 10 or claim 11 whose Final Boiling Point is in the range 240°C to 370°C.
13. A distillate petroleum fuel oil according to any of claims 10 to 12 in which the copolymer is of a di-n-alkyl ester of a dicarboxylic acid in which the alkyl groups containing an average of 12 to 14 carbon atoms and from 10 to 50 wt.% of a vinyl ester, alkyl acrylate or methacrylate.
14. A distillate petroleum fuel oil according to any of claims 10 to 12 containing as a co-additive a polyoxyalkylene ester, ether, ester/ether and mixtures thereof, containing at least two C<sub>10</sub> to C<sub>30</sub> linear saturated alkyl groups and a polyoxyalkylene glycol of molecular weight 100 to 5,000 preferably 200 to 5,000, the alkyl group in said polyoxyalkylene glycol containing from 1 to 4 carbon atoms.

15. A distillate petroleum fuel oil according to any of claims 10 to 12 and 14 containing from 0.5 to 20 parts by weight of the ester copolymer per part of the polyoxyalkylene ester, ether or ester/ether.
16. A distillate petroleum fuel according to any of claims 10 to 12 and 14 also containing any ethylene/unsaturated ester copolymer.

**Claims for the following Contracting State: AT**

1. A process for improving the low temperature properties of a distillate petroleum fuel oil boiling in the range 120°C to 500°C, whose 90% to final boiling point range is 10 to 25°C comprising adding thereto a polymer or copolymer of a di-n-alkyl ester of a mono-ethylenically unsaturated C<sub>4</sub> to C<sub>8</sub> dicarboxylic acid containing at least 25 wt.% of n-alkyl groups wherein the average number of carbon atoms in the n-alkyl groups is from above 12 to 14 and no more than 10 wt.% of alkyl groups in the copolymer containing more than 14 carbon atoms.
2. A process according to claim 1 in which the 20% to 90% distillation points differ by less than 100°C.
3. A process according to claim 1 or claim 2 in which the final boiling point is in the range 340°C to 370°C.
4. A process according to any of claims 1 to 4 in which no more than 20 wt.% of the alkyl group contains fewer than 12 carbon atoms.
5. A process according to any of the preceding claims in which the copolymer is of a di-n-alkyl ester of dicarboxylic acid in which the alkyl groups containing an average of 12 to 14 carbon atoms and from 10 to 50 wt.% of a vinyl ester, an alkyl acrylate or methacrylate.
6. A process according to any of claims 1 to 4 in which there is also added a polyoxyalkylene ester, ether, ester/ether and mixtures thereof, containing at least two C<sub>10</sub> to C<sub>30</sub> linear saturated alkyl groups and a polyoxyalkylene glycol of molecular weight 100 to 5,000 preferably 200 to 5,000, the alkyl group in said polyoxyalkylene glycol containing from 1 to 4 carbon atoms.
7. A process according to any of claims 1 to 4 in which there is also added a polar compound, either ionic or nonionic, which has the capability in fuels of acting as wax crystal growth inhibitors.
8. A process according to claim 8 in which the polar compounds are the amine salts and/or amides formed by reaction of at least one molar proportion of hydrocarbyl-substituted amines with a molar proportion of hydrocarbyl acid having 1 to 4 carboxylic acid groups or their anhydrides containing a total of 30 to 300 carbon atoms.
9. A process according to any of claims 1 to 4 in which there is also added an ethylene/unsaturated ester copolymer.

**Revendications**

**Revendications pour les Etats contractants suivants: BE CH DE FR GB IT LI NL SE**

1. Utilisation pour améliorer les propriétés à basse température d'un fuel-oil de distillation du pétrole, bouillant dans la plage de 120°C à 500°C, dont la plage du point à 90 % d'ébullition au point d'ébullition final va de 10 à 25°C, d'un additif comprenant un polymère ou copolymère d'un ester di-n-alkylique d'un acide dicarboxylique à insaturation monoéthylénique, en C<sub>4</sub> à C<sub>8</sub>, contenant au moins 25 % en poids de groupes n-alkyle dans lequel le nombre moyen d'atomes de carbone dans les groupes n-alkyle va de plus de 12 à 14 et une quantité non supérieure à 10 % en poids des groupes alkyle dans le copolymère contient plus de 14 atomes de carbone.
2. Utilisation suivant la revendication 1, dans laquelle le point à 20 % de distillation et le point à 90 % de distillation diffèrent de moins de 100°C.
3. Utilisation suivant la revendication 1 ou la revendication 2, dans laquelle le point d'ébullition final est

compris dans l'intervalle de 340 ° C à 370 ° C.

4. Utilisation suivant l'une quelconque des revendications 1 à 3, dans laquelle une quantité non supérieure à 20 % en poids des groupes alkyle contient moins de 12 atomes de carbone.
5. Utilisation suivant l'une quelconque des revendications 1 à 4, dans laquelle le copolymère est un copolymère d'un ester di-n-alkylique d'un acide dicarboxylique, dans lequel les groupes alkyle contiennent un nombre moyen d'atomes de carbone de 12 à 14, et de 10 à 50 % en poids d'un ester vinylique ou d'un acrylate ou méthacrylate d'alkyle.
6. Utilisation suivant l'une quelconque des revendications 1 à 4, dans laquelle il est ajouté également un ester, éther, ester/éther de polyoxyalkylène ou un de leurs mélanges, contenant au moins deux groupes alkyle saturés linéaires en C<sub>10</sub> à C<sub>30</sub> et un polyoxyalkylène-glycol d'un poids moléculaire de 100 à 5000, de préférence de 200 à 5000, le groupe alkyle dans ledit polyoxyalkylène-glycol contenant 1 à 4 atomes de carbone.
7. Utilisation suivant l'une quelconque des revendications 1 à 4, dans laquelle il est également ajouté un composé polaire, ionique ou non ionique, qui présente l'aptitude dans des combustibles à jouer le rôle d'inhibiteur de croissance des cristaux de cire.
8. Utilisation suivant la revendication 7, dans laquelle les composés polaires sont les sels d'amines et/ou amides formés par réaction d'au moins une proportion molaire d'amines à substitution hydrocarbyle avec une proportion molaire d'un acide hydrocarbylique ayant 1 à 4 groupes acide carboxylique ou de leurs anhydrides contenant un nombre total d'atomes de carbone de 30 à 300.
9. Utilisation suivant l'une quelconque des revendications 1 à 4, dans laquelle il est ajouté également un copolymère éthylène/ester insaturé.
10. Fuel-oil de distillation du pétrole, bouillant dans la plage de 120 ° C à 500 ° C, dont la plage du point à 90 % d'ébullition au point d'ébullition final va de 10 à 25 ° C, contenant 0,001 à 0,5 % en poids d'un polymère ou copolymère d'un ester di-n-alkylique d'un acide dicarboxylique à insaturation monoéthylénique, en C<sub>4</sub> à C<sub>8</sub>, contenant au moins 25 % en poids de groupes n-alkyle dans lequel le nombre moyen d'atomes de carbone dans les groupes n-alkyle va de plus de 12 à 14, une quantité non supérieure à 10 % en poids de groupes alkyle contenant plus de 14 atomes de carbone dans le copolymère.
11. Fuel-oil de distillation du pétrole suivant la revendication 10, dont le point à 20 % de distillation et le point à 90 % de distillation diffèrent de moins de 100 ° C.
12. Fuel-oil de distillation du pétrole suivant la revendication 10 ou la revendication 11, dont le point d'ébullition final est compris dans l'intervalle de 240 ° C à 370 ° C.
13. Fuel-oil de distillation du pétrole suivant l'une quelconque des revendications 1 à 12, dans lequel le copolymère est un copolymère d'un ester di-n-alkylique d'un acide dicarboxylique, dans lequel les groupes alkyle contiennent un nombre moyen d'atomes de carbone de 12 à 14, et de 10 à 50 % en poids d'un ester vinylique ou d'un acrylate ou méthacrylate d'alkyle.
14. Fuel-oil de distillation du pétrole suivant l'une quelconque des revendications 10 à 12, contenant comme co-additif un ester, éther ou ester/éther de polyoxyalkylène, ou un de leurs mélanges, contenant au moins deux groupes alkyle linéaires saturés en C<sub>10</sub> à C<sub>30</sub> et un polyoxyalkylène-glycol ayant un poids moléculaire de 100 à 5000, de préférence de 200 à 5000, le groupe alkyle dans ledit polyoxyalkylène-glycol contenant 1 à 4 atomes de carbone.
15. Fuel-oil de distillation du pétrole suivant l'une quelconque des revendications 10 à 12 et 14, contenant 0,5 à 20 parties en poids du copolymère d'ester par partie de l'ester, éther ou ester/éther de polyoxyalkylène.
16. Fuel-oil de distillation du pétrole suivant l'une quelconque des revendications 10 à 12 et 14, contenant



également n'importe quel copolymère éthylène/ester insaturé.

#### Revendications pour l'Etat contractant suivant: AT

- 5 1. Procédé pour améliorer les propriétés à basse température d'un fuel-oil de distillation du pétrole, bouillant dans la plage de 120 °C à 500 °C, dont la plage du point à 90 % d'ébullition au point d'ébullition final va de 10 à 25 °C, consistant à y ajouter un polymère ou copolymère d'un ester di-n-alkylique d'un acide dicarboxylique à insaturation monoéthylénique, en C<sub>4</sub> à C<sub>8</sub>, contenant au moins 25 % en poids de groupes n-alkyle dans lequel le nombre moyen d'atomes de carbone dans les groupes  
10 n-alkyle va de plus de 12 à 14 et une quantité non supérieure à 10 % en poids des groupes alkyle dans le copolymère contient plus de 14 atomes de carbone.
2. Procédé suivant la revendication 1, dans lequel le point à 20% de distillation et le point à 90 % de distillation diffèrent de moins de 100 °C.
- 15 3. Procédé suivant la revendication 1 ou la revendication 2, dans lequel le point d'ébullition final est compris dans l'intervalle de 340 °C à 370 °C.
4. Procédé suivant l'une quelconque des revendications 1 à 3, dans lequel une quantité non supérieure à  
20 20 % en poids des groupes alkyle contient moins de 12 atomes de carbone.
5. Procédé suivant l'une quelconque des revendications précédentes, dans lequel le copolymère est un copolymère d'un ester di-n-alkylique d'un acide dicarboxylique, dans lequel les groupes alkyle contiennent un nombre moyen d'atomes de carbone de 12 à 14, et de 10 à 50 % en poids d'un ester  
25 vinylique ou d'un acrylate ou méthacrylate d'alkyle.
6. Procédé suivant l'une quelconque des revendications 1 à 4, dans lequel il est ajouté également un ester, éther, ester/éther de polyoxyalkylène ou un de leurs mélanges, contenant au moins deux groupes alkyle saturés linéaires en C<sub>10</sub> à C<sub>30</sub> et un polyoxyalkylène-glycol d'un poids moléculaire de  
30 100 à 5000, de préférence de 200 à 5000, le groupe alkyle dans ledit polyoxyalkylène-glycol contenant 1 à 4 atomes de carbone.
7. Procédé suivant l'une quelconque des revendications 1 à 4, dans lequel il est également ajouté un composé polaire, ionique ou non ionique, qui présente l'aptitude dans des combustibles à jouer le rôle  
35 d'inhibiteur de croissance des cristaux de cire.
8. Procédé suivant la revendication 7, dans lequel les composés polaires sont les sels d'amines et/ou amides formés par réaction d'au moins une proportion molaire d'amines à substitution hydrocarbyle avec une proportion molaire d'un acide hydrocarbylique ayant 1 à 4 groupes acide carboxylique ou de  
40 leurs anhydrides contenant un nombre total d'atomes de carbone de 30 à 300.
9. Procédé suivant l'une quelconque des revendications 1 à 4, dans lequel il est ajouté également un copolymère éthylène/ester insaturé.

#### 45 Patentansprüche

Patentansprüche für folgende Vertragsstaaten: BE CH DE FR GB IT LI NL SE

1. Verwendung eines Additivs, das ein Polymer oder Copolymer aus einem Di-n-alkylester einer mono-ethylenisch ungesättigten C<sub>4</sub>-C<sub>8</sub>-Dicarbonsäure umfaßt, das mindestens 25 Gew.% an n-Alkylgruppen  
50 enthält, wobei die durchschnittliche Zahl der Kohlenstoffatome in den n-Alkylgruppen etwa 12 bis 14 beträgt und nicht mehr als 10 Gew.% der Alkylgruppen im Copolymer mehr als 14 Kohlenstoffatome enthalten, zur Verbesserung der Eigenschaften eines Erdöldestillatbrennstofföls bei niederen Temperaturen, das im Bereich von 120 °C bis 500 °C siedet und dessen 90% bis Endsiedepunktsbereich 10 bis 25 °C beträgt.
- 55 2. Verwendung nach Anspruch 1, bei der die 20% bis 90% Destillationspunkte um weniger als 100 °C voneinander abweichen.

3. Verwendung nach Anspruch 1 oder 2, bei der der Endsiedepunkt im Bereich von 340 °C bis 370 °C liegt.
4. Verwendung nach einem der Ansprüche 1 bis 3, bei der nicht mehr als 20 Gew.% der Alkylgruppen weniger als 12 Kohlenstoffatome enthalten.
5. Verwendung nach einem der Ansprüche 1 bis 4, bei der das Copolymer aus einem Di-n-alkylester einer Dicarbonsäure, in dem die Alkylgruppen im Durchschnitt 12 bis 14 Kohlenstoffatome aufweisen, und aus 10 bis 50 Gew.% eines Vinylesters, Alkylacrylats oder Methacrylats besteht.
6. Verwendung nach einem der Ansprüche 1 bis 4, bei der außerdem ein Polyoxyalkylenester, -ether, -ester/-ether und Mischungen davon zugegeben wird/werden, der/die mindestens zwei lineare gesättigte C<sub>10</sub>-C<sub>30</sub>-Alkylgruppen und ein Polyoxyalkylenglykol mit einem Molekulargewicht von 100 bis 5000, vorzugsweise 200 bis 5000 aufweist/aufweisen, wobei die Alkylengruppe in dem Polyoxyalkylenglykol 1 bis 4 Kohlenstoffatome enthält.
7. Verwendung nach einem der Ansprüche 1 bis 4, bei der außerdem eine ionische oder nicht-ionische polare Verbindung zugegeben wird, die in Brennstoffen die Fähigkeit hat, als Paraffinkristall-Wachstumsinhibitor zu wirken.
8. Verwendung nach Anspruch 7, bei der die polaren Verbindungen die Aminsalze und/oder Amide sind, die durch Reaktion mindestens eines Mols kohlenwasserstoffsubstituierter Amine mit einem Mol einer Kohlenwasserstoffsäure mit 1 bis 4 Carboxylgruppen oder deren Anhydriden erhalten werden und insgesamt 30 bis 300 Kohlenstoffatome enthalten.
9. Verwendung nach einem der Ansprüche 1 bis 4, bei der außerdem ein Ethylen/ungesättigter Ester-Copolymer zugesetzt wird.
10. Erdöldestillatbrennstofföl, das im Bereich von 120 °C bis 500 °C siedet und dessen 90% bis Endsiedepunktbereich 10 bis 25 °C beträgt, das 0,001 bis 0,5 Gew.% eines Polymeren oder Copolymeren aus einem Di-n-alkylester einer mono-ethylenisch ungesättigten C<sub>4</sub>-C<sub>8</sub>-Dicarbonsäure enthält, das mindestens 25 Gew.% n-Alkylgruppen enthält, wobei die durchschnittliche Zahl der Kohlenstoffatome in den n-Alkylgruppen etwa 12 bis 14 ist und nicht mehr als 10 Gew.% Alkylgruppen im Copolymer vorhanden sind, die mehr als 14 Kohlenstoffatome enthalten.
11. Erdöldestillatbrennstofföl nach Anspruch 10, dessen 20% bis 90% Destillationspunkte sich um weniger als 100 °C unterscheiden.
12. Erdöldestillatbrennstofföl nach Anspruch 10 oder 11, dessen Endsiedepunkt im Bereich von 240 °C bis 370 °C liegt.
13. Erdöldestillatbrennstofföl nach einem der Ansprüche 10 bis 12, bei dem das Copolymer aus einem Di-n-alkylester einer Dicarbonsäure, in dem die Alkylgruppen im Mittel 12 bis 14 Kohlenstoffatome enthalten, und aus 10 bis 50 Gew.% eines Vinylesters, Alkylacrylats oder Methacrylats besteht.
14. Erdöldestillatbrennstofföl nach einem der Ansprüche 10 bis 12, das als Co-Additiv einen Polyoxyalkylenester, -ether, -ester/-ether und Mischungen davon enthält, der/die mindestens zwei lineare gesättigte C<sub>10</sub>-C<sub>30</sub>-Alkylgruppen und ein Polyoxyalkylenglykol mit einem Molekulargewicht von 100 bis 5000, vorzugsweise 200 bis 5000, enthält/enthalten, wobei die Alkylengruppe in dem Polyoxyalkylenglykol 1 bis 4 Kohlenstoffatome enthält.
15. Erdöldestillatbrennstofföl nach einem der Ansprüche 10 bis 12 und 14, das 0,5 bis 20 Gewichtsteile des Ester-Copolymeren pro Gewichtsteil des Polyoxyalkylenesters, -ethers oder -esters/-ethers enthält.
16. Erdöldestillatbrennstofföl nach einem der Ansprüche 10 bis 12 und 14, das außerdem ein Ethylen/ungesättigter Ester-Copolymer enthält.

Patentanspruch für folgenden Vertragsstaat: AT

1. Verfahren zur Verbesserung der Eigenschaften eines Erdöldestillatbrennstofföls bei niedrigen Temperaturen, das im Bereich von 120 °C bis 500 °C siedet und dessen 90% bis Endsiedepunktsbereich 10 bis 25 °C beträgt, bei dem zu dem Öl ein Polymer oder Copolymer aus einem Di-n-alkyl- ester einer mono-ethylenisch ungesättigten C<sub>4</sub>-C<sub>8</sub>-Dicarbonsäure zugegeben wird, das mindestens 25 Gew.% an n-Alkylgruppen enthält, wobei die durchschnittliche Zahl der Kohlenstoffatome der n-Alkylgruppen etwa 12 bis 14 ist und nicht mehr als 10 Gew.% der Alkylgruppen im Copolymer mehr als 14 Kohlenstoffatome enthalten.
2. Verfahren nach Anspruch 1, bei dem die 20% bis 90% Destillationspunkte um weniger als 100 °C voneinander abweichen.
3. Verfahren nach Anspruch 1 oder 2, bei dem der Endsiedepunkt im Bereich von 340 °C bis 370 °C liegt.
4. Verfahren nach einem der Ansprüche 1 bis 3, bei dem nicht mehr als 20 Gew.% der Alkylgruppen weniger als 12 Kohlenstoffatome enthalten.
5. Verfahren nach einem der vorhergehenden Ansprüche, bei dem das Copolymer aus einem Di-n-alkylester einer Dicarbonsäure, in dem die Alkylgruppen im Durchschnitt 12 bis 14 Kohlenstoffatome aufweisen, und aus 10 bis 50 Gew.% eines Vinylesters, Alkylacrylats oder Methacrylats besteht.
6. Verfahren nach einem der Ansprüche 1 bis 4, bei dem außerdem ein Polyoxyalkylenester, -ether, -ester/-ether und Mischungen davon zugegeben wird/werden, der/die mindestens zwei lineare gesättigte C<sub>10</sub>-C<sub>30</sub>-Alkylgruppen und ein Polyoxyalkylenglykol mit einem Molekulargewicht von 100 bis 5000, vorzugsweise 200 bis 5000 aufweist/aufweisen, wobei die Alkylengruppe in dem Polyoxyalkylenglykol 1 bis 4 Kohlenstoffatome enthält.
7. Verfahren nach einem der Ansprüche 1 bis 4, bei dem außerdem eine ionische oder nicht-ionische polare Verbindung zugegeben wird, die in Brennstoffen die Fähigkeit hat, als Paraffinkristall-Wachstumsinhibitor zu wirken.
8. Verfahren nach Anspruch 7, bei dem die polaren Verbindungen die Aminsalze und/oder Amide sind, die durch Reaktion mindestens eines Mols kohlenwasserstoffs substituierter Amine mit einem Mol einer Kohlenwasserstoffsäure mit 1 bis 4 Carboxylgruppen oder deren Anhydriden erhalten werden und insgesamt 30 bis 300 Kohlenstoffatome enthalten.
9. Verfahren nach einem der Ansprüche 1 bis 4, bei dem außerdem ein Ethylen/ungesättigter Ester-Copolymer zugesetzt wird.